

Peristaltic Transport of a Couple-Stress Fluid with Nanoparticles in an Inclined Tube

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Abstract: The paper deals with a theoretical investigation of the peristaltic transport of a couple-stress fluid with heat and mass transfer effects. The velocity, pressure drop, time averaged flux, frictional force, mechanical efficiency, temperature profile, nano particle phenomena, heat transfer coefficient and mass transfer coefficient of the fluid are investigated, when the Reynolds number is small and wave length is large by using appropriate analytical methods. Effects of different physical parameters like couple-stress fluid parameters, Brownian motion parameter, thermophoresis parameter, local temperature Grashof number as well as local nano particle Grashof number on pressure drop characteristics, frictional force, heat transfer coefficient, mass transfer coefficient and stream line patterns of the fluid are studied. The expressions for velocity, temperature profile, nano particle phenomenon, heat transfer coefficient and mass transfer coefficients are sketched through graphs. The streamlines are drawn to discuss trapping phenomenon for some physical quantities.

Keywords: Peristalsis, Couple-stress fluid, Brownian motion parameter, Thermophoresis parameter, Mechanical Efficiency, Heat transfer coefficient, Mass transfer coefficient.

1. Introduction

Peristaltic pumping is a word used to describe a progressive wave of contraction along a tube whose cross-sectional area consequently changes. Peristalsis is an inherent property of many tubular organs of the human body. The mechanism of peristaltic transport has been exploited for industrial applications like sanitary fluid transport, blood pumps in the heart lung machine, transport of corrosive fluids. In view of its importance, a number of researchers investigated peristaltic transport of Newtonian and non-Newtonian fluids under different conditions (Fung & Yih, (1968), Shapiro et al. (1969), Griffiths, (1989), Srinivasacharya et al. (2003), Prasad, Radhakrishnamacharya, & Murthy, (2010), Ellahi et al. (2014), Prasad et al. (2015)).

Couple-stress fluid model has been widely used by researchers because of its relative mathematical simplicity compared with other models. Blood, lubricants containing small amount of high polymer additives, electro-rheological fluids and synthetic fluids show the effect of couple-stress and rotation of

molecules, which are not present in the case of Newtonian fluids. Hence couple-stress fluid serves as a better model for these fluids. Couple-stress fluids was developed by Stokes, (1966). Pal et al. (1988) studied and developed a couple stress model of blood flow in the microcirculation. Effect of peripheral layer on peristaltic transport of a couple-stress fluid was investigated by Prasad & Radhakrishnamacharya, (2009). Maiti & Misra, (2012) studied peristaltic transport of a couple stress fluid: some applications to hemodynamics. Hydromagnetic effect on inclined peristaltic flow of a couple stress fluid was developed by Shit & Roy, (2014).

Nanotechnology has immense contribution in industry since materials of nanometer dimensions exhibit incomparable physical and chemical characteristics. Water, ethylene glycol and oil are common examples of base fluids used for the nanofluid phenomena. Nanofluids have their enormous applications in heat transfer, such as microelectronics, fuel cells, pharmaceutical processes and hybrid powered engines. They explore enhanced thermal conductivity. A large amount of literature is available which deals with the study of nanofluid and its applications. S. U.S. Choi, (1995) was the pioneer to study the nanofluids. Pool boiling of nano-fluids on horizontal narrow tubes was studied by Das et al. (2003). Noreen, (2013) investigated mixed convection peristaltic flow of third order nanofluid with an induced magnetic field. Study of peristaltic motion of nanoparticles of a micropolar fluid with heat and mass transfer effect in an inclined tube was done by Prasad et al. (2015).

It is known that many ducts in physiological system are not horizontal but have some inclination with the axis. Slip effects on peristaltic transport of power-law fluid through an inclined tube was investigated by Naby & Shamy, (2007). Maruthi Prasad & Radhakrishnamacharya, (2008) studied flow of Herschel–Bulkley fluid through an inclined tube of non-uniform cross-section with multiple Stenoses. Shit & Roy, (2014) discussed Hydromagnetic effect on inclined peristaltic flow of a couple -stress fluid. Peristaltic transport of a nanofluid in an inclined tube was investigated by Prasad et al. (2015).

Keeping all the above in view, peristaltic transport of a couple-stress fluid with nanoparticles in an inclined tube has been investigated under the

assumption of long wavelength and low Reynolds number. The coupled equations of temperature profile and nanoparticle phenomena have been solved by using homotopy perturbation method. The analytical solutions of pressure drop, velocity, frictional force, temperature profile and nanoparticle phenomena are obtained. The effects of various parameters on these flow variables have been depicted through graphs.

2. Mathematical Formulation

Consider the peristaltic transport of an incompressible couple stress fluid with nanoparticles in a tube of uniform cross section of radius ‘a’ with sinusoidal wave travelling along the boundary of the tube with speed *c*, amplitude *b* and wave length λ . Further the tube is inclined at an angle α with the horizontal axis. Choosing the cylindrical polar coordinate system (*R, θ, Z*), the wall deformation due to the propagation of an infinite train of peristaltic waves is given by

$$R = H(z, t) = a + b \sin \frac{2\pi}{\lambda} (Z - ct) \tag{1}$$

The governing equations in the fixed frame for an incompressible couple-stress fluid flow with nanoparticles in the absence of body moment and body couple are given as (Maiti et al., (2012))

$$T_{ji,j} = \rho \frac{dw_i}{dt} \tag{2}$$

$$e_{ijk} T_{jk}^A + M_{ji,j} = 0 \tag{3}$$

$$l_{ij} = -p \delta_{ij} + 2\mu_{ij} d_{ij} \tag{4}$$

$$\mu_{ij} = 4\eta \omega_{j,i} + 4\eta' \omega_{ij} \tag{5}$$

$$(\rho c)_f \frac{dT'}{dt} = k \nabla^2 T' + (\rho c)_p [D_B \nabla C' \cdot \nabla T' + \frac{D_T}{T_0} \nabla T' \cdot \nabla T'] \tag{6}$$

$$\frac{dC'}{dt} = D_B \nabla^2 C' + \left[\frac{D_T}{T_0} \right] \nabla^2 T' \tag{7}$$

where w_i is the velocity vector, T_{ij} and T_{ij}^A are the symmetric and antisymmetric parts of the tensor T_{ij} respectively, M_{ij} is the couple-stress tensor, μ_{ij} is the deviatoric part of M_{ij} , ω_{ij} is the vorticity vector, d_{ij} is the symmetric part of the velocity gradient, η and η' are constants associated with the couple-stress, p is the pressure and other terms have their usual meaning from tensor analysis. ρ_f is the density of the fluid, ρ_p is the density of the particle, C is the volumetric volume expansion coefficient, f represents the body forces, $\frac{d}{dt}$ represents the material time derivative, \bar{C} is the nano particle concentration, D_B is the Brownian diffusion coefficient and D_T is the thermophoretic diffusion coefficient. The ambient

values of \bar{T} and \bar{C} as \bar{r} tend to \bar{h} are denoted by \bar{T}_0 and \bar{C}_0 .

Using the transformation

$$r = R, z = Z - ct, u = U, w = W - c, \theta = \theta$$

From a stationary to a moving frame of reference, the equations (2) – (7) are converted to

$$\mu \nabla^2 \left[1 - \frac{1}{\alpha^2} \nabla^2 \right] w' = \frac{dp'}{dz'} + \rho g \beta (T' - T_0') + \rho g \beta (C' - C_0') - \frac{\cos \alpha}{F} \tag{8}$$

$$\left[u' \frac{\partial T'}{\partial r'} + w' \frac{\partial T'}{\partial z'} \right] = \beta \left[\frac{\partial^2 T'}{\partial r'^2} + \frac{1}{r'} \frac{\partial T'}{\partial r'} + \frac{\partial^2 T'}{\partial z'^2} \right] + \tau \left\{ D_B \left[\frac{\partial C'}{\partial r'} \frac{\partial T'}{\partial r'} + \frac{\partial C'}{\partial z'} \frac{\partial T'}{\partial z'} \right] + \frac{D_T}{T_0'} \left[\left(\frac{\partial T'}{\partial r'} \right)^2 + \left(\frac{\partial T'}{\partial z'} \right)^2 \right] \right\} \tag{9}$$

$$\left[u' \frac{\partial C'}{\partial r'} + w' \frac{\partial C'}{\partial z'} \right] = D_B \left[\frac{\partial^2 C'}{\partial r'^2} + \frac{1}{r'} \frac{\partial C'}{\partial r'} + \frac{\partial^2 C'}{\partial z'^2} \right] + \frac{D_T}{T_0'} \left[\frac{\partial^2 T'}{\partial r'^2} + \frac{1}{r'} \frac{\partial T'}{\partial r'} + \frac{\partial^2 T'}{\partial z'^2} \right] \tag{10}$$

$$\text{with } \nabla^2 = \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial}{\partial r} \right)$$

where $\tau = \frac{(\rho c)_p}{(\rho c)_f}$ is the ratio between the effective heat capacity of the nanoparticle material and heat capacity of the fluid.

Introducing the following non-dimensional quantities:

$$r = \frac{r'}{a}, \quad z = \frac{z'}{\lambda}, \quad w = \frac{w'}{c}, \quad p = \frac{a^2 p'}{\lambda c \mu},$$

$$t = \frac{ct'}{\lambda}, \quad u = \frac{\lambda u'}{ac}, \quad \theta_t = \frac{T' - T_0'}{T_0'}$$

$$\delta = \frac{a}{\lambda}, \quad Re = \frac{2\rho c a}{\mu}, \quad \sigma = \frac{C' - C_0'}{C_0'}$$

$$\beta = \frac{k}{(\rho c)_f}, \quad Nb = \frac{(\rho c)_p D_B C_0'}{(\rho c)_f}$$

$$N_t = \frac{(\rho c)_p D_T T_0'}{(\rho c)_f \beta}, \quad Gr = \frac{g \beta a^3 T_0'}{\gamma^2}$$

$$Br = \frac{g \beta a^3 C_0'}{\gamma^2}$$

$$\bar{\alpha} = \alpha a = \sqrt{\frac{\mu}{\eta}} a, \quad h' = \frac{h}{a}$$

Using the non-dimensional quantities in equations (8)-(10) and applying the long wavelength and low Reynolds number approximations and neglecting the inertial terms, the equations (8)-(10) are converted to

$$\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial}{\partial r} \left(1 - \frac{1}{\alpha^2} \nabla^2 \right) w \right) = \frac{dp}{dz} + G_r \theta_t + B_r \sigma - \frac{\cos \alpha}{F} \tag{11}$$

$$0 = \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial \theta_t}{\partial r} \right) + N_b \frac{\partial \sigma}{\partial r} \frac{\partial \theta_t}{\partial r} + N_t \left(\frac{\partial \theta_t}{\partial r} \right)^2 \tag{12}$$

$$0 = \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial \sigma}{\partial r} \right) + \frac{N_t}{N_b} \left(\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial \theta_t}{\partial r} \right) \right) \tag{13}$$

where N_b, N_t, G_r, B_r are the Brownian motion parameter, Thermophoresis parameter, local temperature Grashof number and local nano particle Grashof number, and w is the axial velocity, r is the

radial coordinate, $\bar{\alpha}$ is the couple-stress fluid parameter, θ_t is the temperature profile and σ is the nano particle phenomenon.

The non-dimensional boundary conditions are:

$$\frac{\partial w}{\partial r} = 0, \frac{\partial \theta_t}{\partial r} = 0, \frac{\partial \sigma}{\partial r} = 0 \text{ at } r = 0(14)$$

$$w = -1, \theta_t = 0, \sigma = 0 \text{ at } r = h(z) = 1 + \varepsilon \sin 2\pi z \quad (15)$$

$$\frac{\partial^2 w}{\partial r^2} - \frac{\eta}{r} \frac{\partial w}{\partial r} = 0 \text{ at } r = h(z) = 1 + \varepsilon \sin 2\pi z(16)$$

$$\frac{\partial^2 w}{\partial r^2} - \frac{\eta}{r} \frac{\partial w}{\partial r} \text{ is finite at } r = 0. \quad (17)$$

where $\varepsilon (= \frac{b}{a})$ is the amplitude ratio and $\eta' = \frac{\eta}{\eta}$ is a couple-stress fluid parameter.

Boundary conditions (16) and (17) indicate that the couple-stresses vanish at the tube wall and is finite at the tube axis respectively.

3. Solution of the Problem

Homotopy perturbation method is a combination of homotopy method and perturbation method. Homotopy perturbation method is more appropriate method than the other traditional perturbation methods. By using this method we will overcome the drawbacks of the traditional perturbation methods.

The homotopy for the equations (12) and (13) are as follows Akbar & Nadeem, (2013):

$$H(\zeta, \theta_t) = (1 - \zeta)[L(\theta_t) - L(\theta_{t10})] + \zeta \left[L(\theta_t) + N_b \frac{\partial \sigma}{\partial r} \frac{\partial \theta_t}{\partial r} + N_t \left(\frac{\partial \theta_t}{\partial r} \right)^2 \right] \quad (18)$$

$$H(\zeta, \sigma) = (1 - \zeta)[L(\sigma) - L(\sigma_{10})] + \zeta \left[L(\sigma) + \frac{N_t}{N_b} \left(\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial \theta_t}{\partial r} \right) \right) \right] \quad (19)$$

where $L = \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial}{\partial r} \right)$ is taken as linear operator for convenience.

$$\theta_{t10}(r, z) = \left(\frac{r^2 - h^2}{4} \right), \quad \sigma_{10}(r, z) = - \left(\frac{r^2 - h^2}{4} \right) \left(\frac{N_t}{N_b} \right) \quad (20)$$

are defined as initial guesses which satisfy the boundary conditions.

Define

$$\theta_t(r, z) = \theta_{t0} + \zeta \theta_{t1} + \zeta^2 \theta_{t2} + \dots \quad (21)$$

$$\sigma(r, z) = \sigma_0 + \zeta \sigma_1 + \zeta^2 \sigma_2 + \dots \quad (22)$$

The series (21) and (22) are convergent for most of the cases. The convergent rate depends on the nonlinear part of the equation.

Adopting the same procedure as done by Akbar & Nadeem, (2013), the solution for temperature profile and nano particle phenomena can be written for $\zeta = 1$ as

$$\theta_t(r, z) = N_t \left(\frac{r^3 - h^3}{18} \right) - (N_b + N_t) \left(\frac{r^4 - h^4}{64} \right) + N_b N_t \left(\frac{r^5 - h^5}{300} \right) - N_b N_t \left(\frac{r^6 - h^6}{1152} \right) \quad (23)$$

$$\sigma(r, z) = - \left(\frac{r^2 - h^2}{4} \right) \frac{N_t}{N_b} + \left(\frac{r^2 - h^2}{4} \right) \frac{N_t}{N_b} - \frac{N_t^2}{N_b} \left(\frac{r^3 - h^3}{18} \right) + \frac{N_t^2}{N_b} \left(\frac{r^4 - h^4}{64} \right) \quad (24)$$

Substituting Eqs. (23) and (24) in Eq. (11), it can be written as

$$\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial}{\partial r} \left(1 - \frac{1}{\bar{\alpha}} \nabla^2 \right) w \right) = \frac{dp}{dz} - \frac{\cos \alpha}{F} + G_r N_t \left(\frac{r^3 - h^3}{18} \right) - G_r (N_b + N_t) \left(\frac{r^4 - h^4}{64} \right) + G_r N_b N_t \left(\frac{r^5 - h^5}{300} \right) - G_r N_b N_t \left(\frac{r^6 - h^6}{1152} \right) - B_r \left(\frac{r^2 - h^2}{4} \right) \frac{N_t}{N_b} + B_r \left(\frac{r^2 - h^2}{4} \right) \frac{N_t}{N_b} - B_r \frac{N_t^2}{N_b} \left(\frac{r^3 - h^3}{18} \right) + B_r \frac{N_t^2}{N_b} \left(\frac{r^4 - h^4}{64} \right) \quad (25)$$

Solving Eq. (25) subject to the boundary conditions (14)- (17), the expression for velocity is given as

$$w = -1 + S_1 \left(I_0(\bar{\alpha}r) - I_0(\bar{\alpha}h) \right) + \frac{dp}{dz} \left[\left(\frac{\eta - 1}{2A} \right) \left(I_0(\bar{\alpha}r) - I_0(\bar{\alpha}h) \right) + \frac{r^2 - h^2}{4} \right] - \frac{\cos \alpha}{F} \left[\left(\frac{\eta - 1}{2A} \right) \left(I_0(\bar{\alpha}r) - I_0(\bar{\alpha}h) \right) + \frac{r^2 - h^2}{4} \right] + G_r N_t \left[\frac{r^3 - h^3}{18\bar{\alpha}^2} + \frac{r - h}{50\bar{\alpha}^4} + \frac{r^5}{450} - \frac{r^2 h^3}{72} + \frac{7h^5}{600} \right] + G_r (N_b + N_t) \left[\frac{r^4 - h^4}{64\bar{\alpha}^2} + \frac{r^2 - h^2}{4\bar{\alpha}^4} + \frac{r^4}{64\bar{\alpha}^2} - \frac{r^2 h^4}{256} + \frac{r^6}{2304} + \frac{h^6}{288} \right] + G_r N_b N_t \left[\frac{3(r - h)}{4\bar{\alpha}^6} + \frac{r^2 - h^2}{2\bar{\alpha}^6} + \frac{r^3 - h^3}{12\bar{\alpha}^4} - \frac{r^4 - h^4}{32\bar{\alpha}^4} + \frac{r^5 - h^5}{300\bar{\alpha}^2} - \frac{r^6 - h^6}{r^2 h^6} - \frac{r^2 h^5}{r^8} - \frac{1200}{14700} + \frac{4608}{h^7} - \frac{73728}{5h^8} - \frac{14700}{14700} + \frac{1200}{1200} - \frac{24576}{24576} \right] + B_r \left(\frac{N_t}{N_b} - 1 \right) \left[\frac{r^2 - h^2}{\bar{\alpha}^2} + \frac{r^4 - h^4}{16} + \frac{r^2 h^2}{16} \right] + B_r \left(\frac{N_t^2}{N_b} \right) \left[- \frac{r - h}{2\bar{\alpha}^4} + \frac{3(r^2 - h^2)}{2\bar{\alpha}^4} - \frac{r^3 - h^3}{18\bar{\alpha}^2} + \frac{3(r^4 - h^4)}{32\bar{\alpha}^2} + \frac{r^6 - h^6}{384} + \frac{r^2 h^3}{72} - \frac{r^5}{450} - \frac{r^2 h^5}{256} - \frac{7h^5}{600} + \frac{h^7}{256} \right] \quad (26)$$

where

$$A = \bar{\alpha} \left[\bar{\alpha} I_0(\bar{\alpha}h) - \left(\frac{1+\eta}{h} \right) I_1(\bar{\alpha}h) \right] \text{ and}$$

$$S_1 = -\frac{G_r N_t}{A} \left[\frac{-h^3}{36} (1 + \bar{\eta}) + \frac{h}{3\bar{\alpha}^2} \left(1 - \frac{\bar{\eta}}{2} \right) + \frac{2h^3}{45} \right. \\ \left. - \frac{\bar{\eta}}{50\bar{\alpha}^4 h} - \frac{\bar{\eta} h^3}{90} \right] \\ - \frac{G_r (N_b + N_t)}{A} \left[\frac{1}{2\bar{\alpha}^4} - \frac{\bar{\eta}}{2\bar{\alpha}^4} \right. \\ \left. + \frac{h^4 (1 - \bar{\eta})}{192} + \frac{h^2 (3 - \bar{\eta})}{16\bar{\alpha}^2} \right] \\ - \frac{G_r N_b N_t}{A} \left[\frac{h^5 (\bar{\eta} - 1)}{600} - \frac{(1 + \bar{\eta})}{\bar{\alpha}^6} \right. \\ \left. + \frac{h \left(1 - \frac{\bar{\eta}}{2} \right)}{2\bar{\alpha}^4} + \frac{h^3 \left(1 - \frac{\bar{\eta}}{4} \right)}{15\bar{\alpha}^2} \right. \\ \left. + \frac{h^4 \left(1 - \frac{\bar{\eta}}{5} \right)}{490} + \frac{h^6 (1 - \bar{\eta})}{2304} \right. \\ \left. + \frac{h^2 (\bar{\eta} - 3)}{8\bar{\alpha}^4} + \frac{h^4 (\bar{\eta} - 5)}{192\bar{\alpha}^2} \right. \\ \left. + \frac{h^6 (\bar{\eta} - 7)}{9216} - \frac{3\bar{\eta}}{4h\bar{\alpha}^6} \right] \\ - \frac{B_r (N_t - 1)}{A (N_b)} \left[\frac{2(1 - \bar{\eta})}{\bar{\alpha}^2} \right. \\ \left. + \frac{h^2 (1 - \bar{\eta})}{8} + \frac{3h^2 (1 - \bar{\eta})}{4} \right] \\ - \frac{B_r N_t^2}{A N_b} \left[\frac{h^3 (1 - \bar{\eta})}{36} + \frac{h \left(-2 + \frac{\bar{\eta}}{8} \right)}{6\bar{\alpha}^2} \right. \\ \left. + \frac{h^3 (\bar{\eta} + 4)}{90} + \frac{3(1 - \bar{\eta})}{\bar{\alpha}^4} \right. \\ \left. + \frac{h^5 (\bar{\eta} - 1)}{128} + \frac{h^2 (9 - 3\bar{\eta})}{8\bar{\alpha}^2} \right. \\ \left. + \frac{h^4 (5 - \bar{\eta})}{64} + \frac{\bar{\eta}}{2h\bar{\alpha}^4} \right]$$

The dimensionless flux in the moving frame is given as

$$q = \int_0^h 2r w dr \quad (27)$$

Substituting Eq. (26) in Eq. (27) and solving, the flux is

$$q = -h^2 + 2S_1 S + \frac{dp}{dz} \left[\left(\left(\frac{\bar{\eta} - 1}{A} \right) S \right) - \frac{h^4}{8} \right] \\ - \frac{\cos \alpha}{F} \left[\left(\left(\frac{\bar{\eta} - 1}{A} \right) S \right) - \frac{h^4}{8} \right] \\ + G_r N_t \left[\frac{-h^5}{30\bar{\alpha}^2} - \frac{h^3}{150\bar{\alpha}^4} + \frac{3h^7}{560} \right] + G_r (N_b + N_t) \\ \left[\frac{-h^6}{192\bar{\alpha}^2} - \frac{h^4}{8\bar{\alpha}^4} + \frac{5h^8}{3072} \right] + G_r N_b N_t \left[\frac{-h^3}{4\bar{\alpha}^6} + \right. \\ \left. \frac{-h^4}{4\bar{\alpha}^6} - \frac{h^5}{20\bar{\alpha}^4} + \frac{h^6}{48\bar{\alpha}^4} + \frac{h^8}{1536\bar{\alpha}^2} - \frac{h^8}{19600} + \frac{h^9}{2400} - \right. \\ \left. \frac{h^{10}}{10240} \right] + B_r \left(\frac{N_t}{N_b} - 1 \right) \left[\frac{-h^4}{2\bar{\alpha}^2} + \frac{5h^6}{96} - \right. \\ \left. \frac{2h^7}{16} \right] + B_r \left(\frac{N_t^2}{N_b} \right) \left[\frac{-h^3}{\bar{\alpha}^4} - \frac{3(h^4)}{2\bar{\alpha}^4} + \frac{4h^5}{45\bar{\alpha}^2} - \frac{h^6}{16\bar{\alpha}^2} - \right.$$

$$\left. \frac{3h^7}{360} - \frac{293h^8}{149376} + \frac{h^9}{512} \right] \quad (28)$$

where $S = hI_1(\bar{\alpha}h) - \frac{h^2}{2} I_0(\bar{\alpha}h)$

From Eq. (28), the expression for $\frac{dp}{dz}$ is

$$\frac{dp}{dz} = \frac{-1}{S_0} q + \frac{\cos \alpha}{F} - \frac{h^2}{S_0} + \frac{2S_1 S}{S_0} \\ + \frac{G_r N_t}{S_0} \left[\frac{-h^5}{30\bar{\alpha}^2} - \frac{h^3}{150\bar{\alpha}^4} + \frac{3h^7}{560} \right] \\ + \frac{G_r (N_b + N_t)}{S_0} \left[\frac{-h^6}{192\bar{\alpha}^2} - \frac{h^4}{8\bar{\alpha}^4} \right. \\ \left. + \frac{5h^8}{3072} \right] \\ + \frac{G_r N_b N_t}{S_0} \left[\frac{-h^3}{4\bar{\alpha}^6} + \frac{-h^4}{4\bar{\alpha}^6} - \frac{h^5}{20\bar{\alpha}^4} + \frac{h^6}{48\bar{\alpha}^4} + \frac{h^8}{1536\bar{\alpha}^2} \right. \\ \left. - \frac{h^8}{19600} + \frac{h^9}{2400} - \frac{h^{10}}{10240} \right] \\ + \frac{B_r (N_t - 1)}{S_0 (N_b)} \left[\frac{-h^4}{2\bar{\alpha}^2} + \frac{5h^6}{96} - \frac{2h^7}{16} \right] \\ + \frac{B_r (N_t^2)}{S_0 (N_b)} \left[\frac{-h^3}{\bar{\alpha}^4} - \frac{3(h^4)}{2\bar{\alpha}^4} + \frac{4h^5}{45\bar{\alpha}^2} - \frac{h^6}{16\bar{\alpha}^2} - \frac{3h^7}{360} - \right. \\ \left. \frac{293h^8}{149376} + \frac{h^9}{512} \right] \quad (29)$$

where $S_0 = \frac{h^4}{8} - \left(\frac{\bar{\eta} - 1}{A} \right) S$

The pressure drop over the wavelength ΔP_λ is defined as

$$\Delta P_\lambda = - \int_0^1 \frac{dp}{dz} dz. \quad (30)$$

Substituting the expression $\frac{dp}{dz}$ in Eq. (30), the pressure drop is

$$\Delta P_\lambda = qL_1 + L_2 \quad (31)$$

where $L_1 = \int_0^1 \frac{1}{S_0} dz$

$$(32)$$

and

$$L_2 = \int_0^1 \left(\frac{h^2}{S_0} - \frac{2S_1 S}{S_0} + \frac{\cos \alpha}{F} - \frac{G_r N_t}{S_0} \left[\frac{-h^5}{30\bar{\alpha}^2} - \frac{h^3}{150\bar{\alpha}^4} + \right. \right. \\ \left. \left. \frac{3h^7}{560} \right] - \frac{G_r (N_b + N_t)}{S_0} \left[\frac{-h^6}{192\bar{\alpha}^2} - \frac{h^4}{8\bar{\alpha}^4} + \frac{5h^8}{3072} \right] - \frac{G_r N_b N_t}{S_0} \left[\frac{-h^3}{4\bar{\alpha}^6} + \right. \right. \\ \left. \left. \frac{-h^4}{4\bar{\alpha}^6} - \frac{h^5}{20\bar{\alpha}^4} + \frac{h^6}{48\bar{\alpha}^4} + \frac{h^8}{1536\bar{\alpha}^2} - \frac{h^8}{19600} + \frac{h^9}{2400} - \frac{h^{10}}{10240} \right] - \right. \\ \left. \frac{B_r (N_t - 1)}{S_0 (N_b)} \left[\frac{-h^4}{2\bar{\alpha}^2} + \frac{5h^6}{96} - \frac{2h^7}{16} \right] - \frac{B_r (N_t^2)}{S_0 (N_b)} \left[\frac{-h^3}{\bar{\alpha}^4} - \right. \right. \\ \left. \left. \frac{3(h^4)}{2\bar{\alpha}^4} + \frac{4h^5}{45\bar{\alpha}^2} - \frac{h^6}{16\bar{\alpha}^2} - \frac{3h^7}{360} - \frac{293h^8}{149376} + \frac{h^9}{512} \right] \right) dz \quad (33)$$

Following the analysis of Shapiro et al.(1969), the time averaged flux over a period in the laboratory frame \bar{Q} is given as

$$\bar{Q} = 1 + \frac{\epsilon^2}{2} + q \quad (34)$$

Substituting Eq. (31) in equation Eq. (34), the time averaged flux is

$$\bar{Q} = 1 + \frac{\epsilon^2}{2} + \frac{\Delta P_\lambda}{L_1} - \frac{L_2}{L_1} \quad (35)$$

The dimensionless frictional force \bar{F} at the wall is

$$\bar{F} = \int_0^1 h^2 \left(-\frac{dp}{dz} \right) dz \quad (36)$$

Heat Transfer Coefficient

The heat transfer coefficient at the wall is given as

$$Z_\theta(r, z) = \left(\frac{\partial h}{\partial z}\right) \left(\frac{\partial \theta_t}{\partial r}\right) \tag{37}$$

Mass Transfer Coefficient

The mass transfer coefficient at the wall is as follows

$$Z_\sigma(r, z) = \left(\frac{\partial h}{\partial z}\right) \left(\frac{\partial \sigma}{\partial r}\right) \tag{38}$$

4. Results and Discussion

Analytical expressions for the pressure drop, time averaged flux, frictional force, heat transfer coefficient and mass transfer coefficient have been calculated. Various graphs are depicted by using Mathematica software.

4.1 Pressure drop characteristics

Figs. 1.1-1.7 illustrate the variation of pressure drop (Δp_λ) with time averaged flux (\bar{Q}) of peristaltic waves for different values of couple-stress fluid parameters $\bar{\alpha}, \bar{\eta}$, Brownian motion parameter (N_b), thermophoresis parameter (N_t), local temperature Grashof number (G_r), local nano particle Grashof number (B_r) and inclination (α).

From Fig. 1.1, 1.3, 1.5 and 1.7 it is clear that pressure drop (Δp_λ) increases with the couple-stress fluid parameter $\bar{\alpha}$, Brownian motion parameter (N_b), local temperature Grashof number (G_r) and with inclination (α). It is observed from Fig 1.2 that pressure drop (Δp_λ) increases with the couple-stress fluid parameter $\bar{\eta}$ in the peristaltic pumping region ($0 < \bar{Q} < 0.38$) and decreases in the augmented pumping region ($0.42 < \bar{Q} < 1$). From Figs. 1.4 & 1.6, it is noticed that as the time averaged flux (\bar{Q}) increases, pressure drop (Δp_λ) decreases with the increase of thermophoresis parameter (N_t) and with the local nano particle Grashof number (B_r).

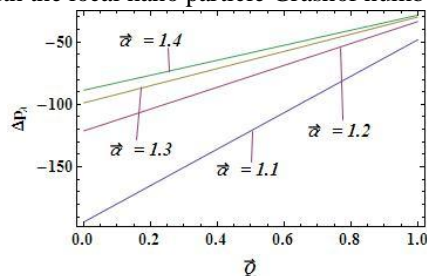


Fig.1.1: Effect of \bar{Q} and $\bar{\alpha}$ on (Δp_λ)

($\epsilon = 0.9, \bar{\eta} = 0.2, G_r = 0.5, B_r = 0.3, N_b = 1.3, N_t = 1.8, \alpha = 30^\circ$)

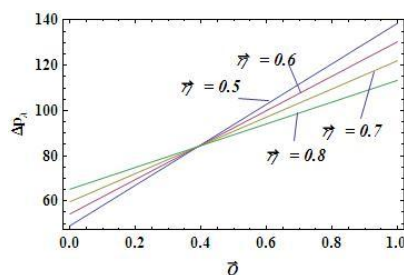


Fig.1.2: Effect of \bar{Q} and $\bar{\eta}$ on (Δp_λ)

($\epsilon = 0.4, \bar{\alpha} = 1, G_r = 0.5, B_r = 0.3, N_b = 1.3, N_t = 1.8, \alpha = 30^\circ$)

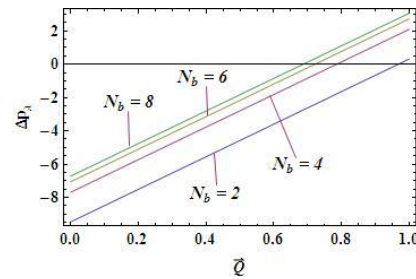


Fig.1.3: Effect of \bar{Q} and N_b on (Δp_λ)

($\epsilon = 0.1, \bar{\alpha} = 3.2, \bar{\eta} = 1.2, G_r = 0.5, B_r = 0.3, N_t = 1.8, \alpha = 30^\circ$)

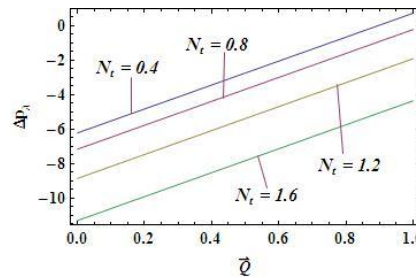


Fig.1.4: Effect of \bar{Q} and N_t on (Δp_λ)

($\epsilon = 0.1, \bar{\alpha} = 1.2, \bar{\eta} = 0.8, G_r = 0.5, B_r = 0.3, N_b = 1.3, \alpha = 30^\circ$)

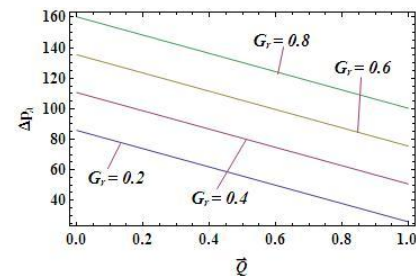


Fig.1.5: Effect of \bar{Q} and G_r on (Δp_λ)

($\epsilon = 0.3, \bar{\alpha} = 2.2, \bar{\eta} = 1.8, N_b = 1.3, B_r = 0.3, N_t = 1.8, \alpha = 30^\circ$)

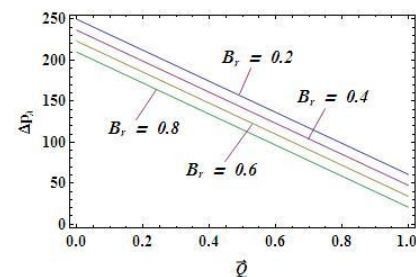


Fig.1.6: Effect of \bar{Q} and B_r on (Δp_λ)

($\epsilon = 0.9, \bar{\alpha} = 2.2, \bar{\eta} = 0.8, G_r = 0.5, N_b = 1.3, N_t = 1.8, \alpha = 30^\circ$)

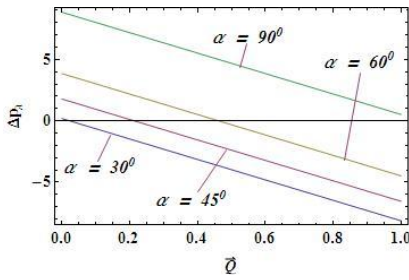


Fig.1.7: Effect of \bar{Q} and α on (Δp_λ)

($\epsilon = 0.9, \bar{\alpha} = 2.2, \bar{\eta} = 0.8, G_r = 0.5, N_b = 1.3, N_t = 1.8, B_r = 0.3$)

4.2 Frictional Force

The variation of absolute value of the frictional force ($|\bar{F}|$) with various parameters is shown graphically from Figs. 2.1-2.7. The frictional force ($|\bar{F}|$) increases with couple-stress fluid parameter $\bar{\eta}$, thermophoresis parameter (N_t) and with local Nano particle Grashof number (B_r) but decreases with Brownian motion parameter (N_b), local temperature Grashof number (G_r) and with inclination (α).

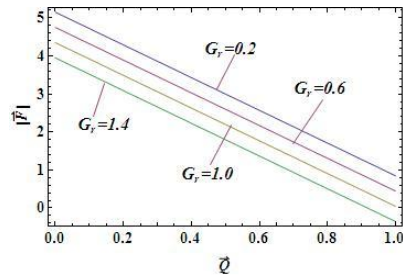


Fig.2.4: Effect of \bar{Q} and G_r on \bar{F}

($\epsilon = 0.1, \bar{\alpha} = 1.8, \bar{\eta} = 1.5, N_b = 1.3, B_r = 0.3, N_t = 1.8, \alpha = 30^\circ$)

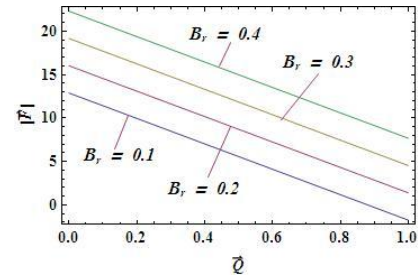


Fig.2.5: Effect of \bar{Q} and B_r on \bar{F}

($\epsilon = 0.1, \bar{\alpha} = 0.8, \bar{\eta} = 0.5, G_r = 0.5, N_b = 1.3, N_t = 1.8, \alpha = 30^\circ$)

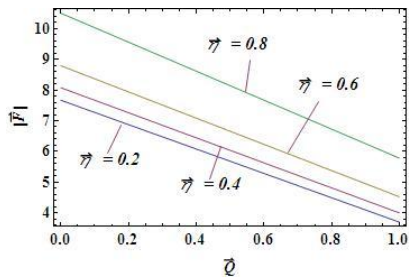


Fig.2.1: Effect of \bar{Q} and $\bar{\eta}$ on \bar{F}

($\epsilon = 0.9, \bar{\alpha} = 1.8, G_r = 0.5, B_r = 0.3, N_b = 1.3, N_t = 1.8, \alpha = 30^\circ$)

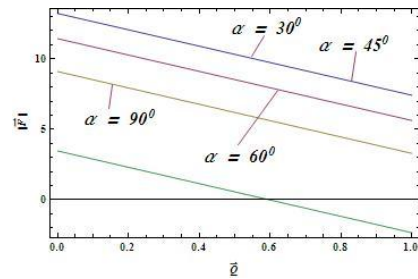


Fig.2.6: Effect of \bar{Q} and α on \bar{F}

($\epsilon = 0.1, \bar{\alpha} = 0.8, \bar{\eta} = 0.5, G_r = 0.5, N_b = 1.3, N_t = 1.8, B_r = 0.3$)

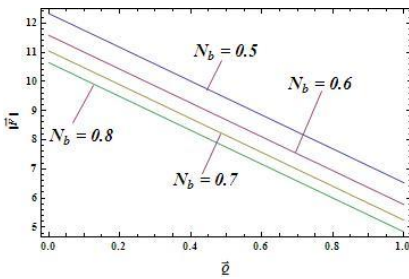


Fig.2.2: Effect of \bar{Q} and N_b on \bar{F}

($\epsilon = 0.5, \bar{\eta} = 0.2, G_r = 0.5, B_r = 0.3, \bar{\alpha} = 1.2, N_t = 1.8, \alpha = 30^\circ$)

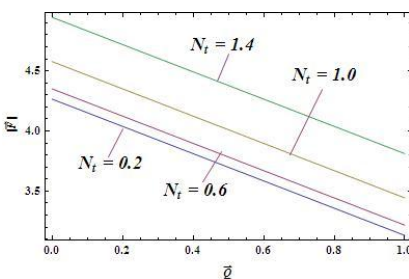


Fig.2.3: Effect of \bar{Q} and N_t on \bar{F}

($\epsilon = 0.5, \bar{\alpha} = 3.2, \bar{\eta} = 1.2, G_r = 0.5, B_r = 0.3, N_b = 1.3, \alpha = 30^\circ$)

4.3 Temperature Profile

Effects of temperature profile (θ_t) with respect to the Brownian motion parameter (N_b) and thermophoresis parameter (N_t) has been shown from Figs. 4.1-4.2. It can be seen that, temperature profile (θ_t) increases with the increase of Brownian motion parameter (N_b) and decreases with the increase of thermophoresis parameter (N_t). It is interesting to observe that value of temperature profile (θ_t) is maximum in the range $[-0.5, 0.5]$.

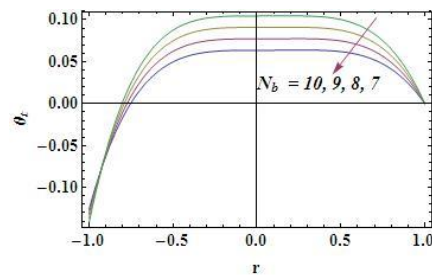


Fig. 3.1: Variation in Temperature profile with N_b

($z = 2, \epsilon = 0.1, N_t = 0.8$)

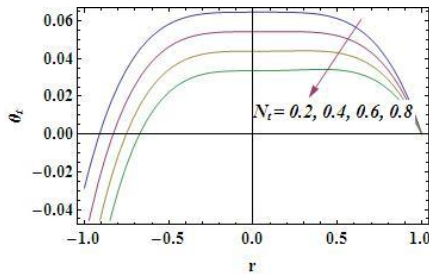


Fig. 3.2: Variation in Temperature profile with N_t
($z = 2, \epsilon = 0.1, N_b = 4.8$)

4.4 Nanoparticle phenomena

Figs. 4.1-4.2 explain the nature of nanoparticle phenomena (σ) for different values of Brownian motion parameter (N_b) and thermophoresis parameter (N_t). It can be seen that, the nano particle phenomena (σ) increases with the increase of Brownian motion parameter (N_b) and decreases with the increase of thermophoresis parameter (N_t). It is also observed that nano particle phenomena (σ) attains maximum value at $r = 0$.

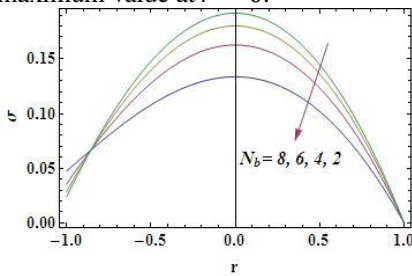


Fig. 4.1: Variation in Nano particle with N_b
($z = 2, \epsilon = 0.1, N_t = 0.8$)

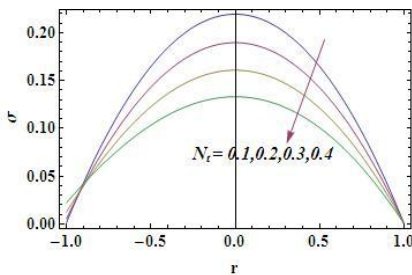


Fig. 4.2: Variation in Nano particle with N_t
($z = 2, \epsilon = 0.1, N_b = 0.3$)

4.5 Heat Transfer Coefficient

Figs. 5.1-5.3 indicate the variation of heat transfer coefficient (Z_θ) for various values of Brownian motion parameter (N_b), thermophoresis parameter (N_t) and amplitude ratio (ϵ). From Figs. 5.1-5.3, it can be observed that, the value of the heat transfer coefficient (Z_θ) increases with Brownian motion parameter (N_b) and thermophoresis parameter (N_t), amplitude ratio (ϵ) and then decreases after attaining a constant value.

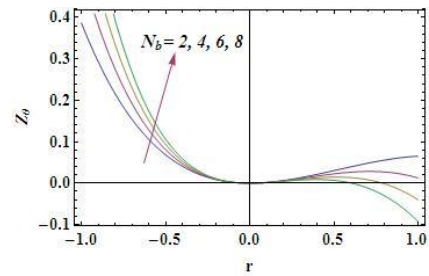


Fig. 5.1: Variation in heat transfer coefficient with N_b
($z = 2, \epsilon = 0.1, N_t = 1.8$)

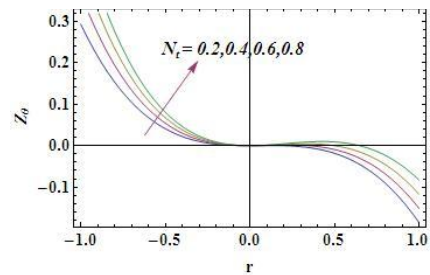


Fig. 5.2: Variation in heat transfer coefficient with N_t
($z = 2, \epsilon = 0.2, N_b = 2.8$)

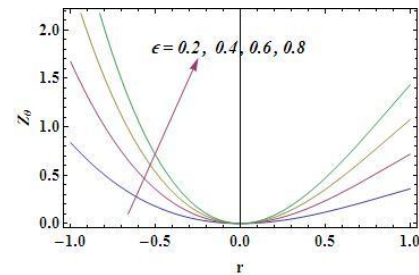


Fig. 5.3: Variation in heat transfer coefficient with ϵ
($z = 2, N_t = 2.8, N_b = 0.2$)

4.6 Mass Transfer Coefficient

Figs. 6.1-6.3 illustrate the effect of various parameters on mass transfer coefficient (Z_σ). It is interesting to observe that, mass transfer coefficient (Z_σ) increases with Brownian motion parameter (N_b), thermophoresis parameter (N_t) and with amplitude ratio (ϵ) and then decreases after attaining a constant value.

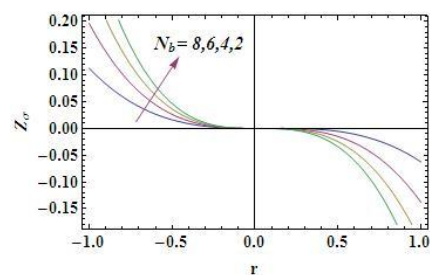


Fig. 6.1: Variation in Mass transfer coefficient with N_b
($z = 2, \epsilon = 0.1, N_t = 0.2$)

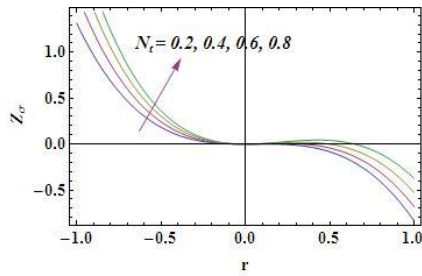


Fig. 6.2: Variation in Mass transfer coefficient with N_t
($z = 2, \epsilon = 0.9, N_b = 2.8$)

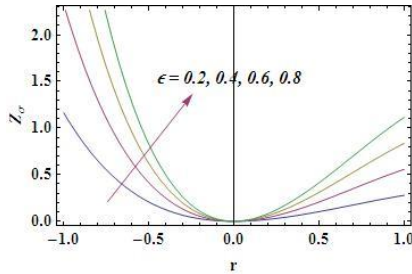


Fig. 6.3: Variation in Mass transfer coefficient with ϵ
($z = 2, N_t = 2.8, N_b = 2.3$)

4.7 Streamline patterns

Trapping is a phenomenon where the streamlines on the center line in the moving frame are divided in order to encircle a bolus of fluid particles circulating along closed streamlines under certain given conditions. Trapping is a characteristic of peristaltic motion. As the bolus emanate to be trapped by the wave, the bolus moves at equal speed with that of the wave. Figs. 7.1-7.4 illustrates the streamline patterns and trapping for different values of couple-stress fluid parameters, Brownian motion parameter and local nano particle Grashof number.

From Fig. 7.1 it is clear that, the size of the trapped bolus decreases first and then increases with the increases of couple-stress fluid parameter $\bar{\alpha}$. It is observed from Fig. 7.2 that, the size of the trapped bolus increases with the increase of couple-stress fluid parameter $\bar{\eta}$. From Fig. 7.3 it is noticed that, the size of the trapped bolus decreases with the increase of Brownian motion parameter (N_b). It is interesting to observe from Fig. 7.4 that, the size of the upper bolus increases and the size of the lower bolus decreases with the increase of local nanoparticle Grashof number (B_r).

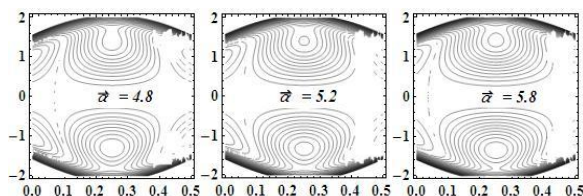


Fig.7.1: Stream line patterns for different values of $\bar{\alpha}$
($\epsilon = 0.5, \bar{Q} = 0.7, \bar{\eta} = 1.1, G_r = 6, B_r = 5, N_b = 10, N_t = 5, \alpha = 30^0$)

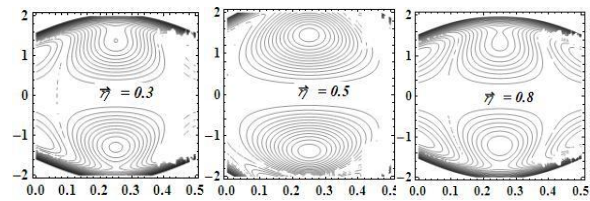


Fig.7.2: Stream line patterns for different values of $\bar{\eta}$
($\epsilon = 0.5, \bar{Q} = 0.7, \bar{\alpha} = 5, G_r = 6, B_r = 5, N_b = 10, N_t = 5, \alpha = 30^0$)

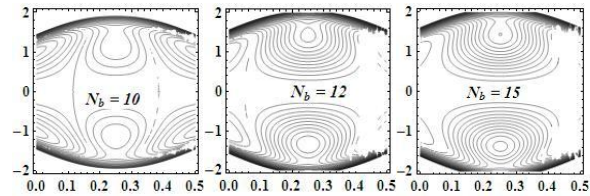


Fig.7.3: Stream line patterns for different values of N_b
($\epsilon = 0.5, \bar{Q} = 0.7, \bar{\alpha} = 5, G_r = 6, B_r = 5, \bar{\eta} = 1.1, N_t = 5, \alpha = 30^0$)

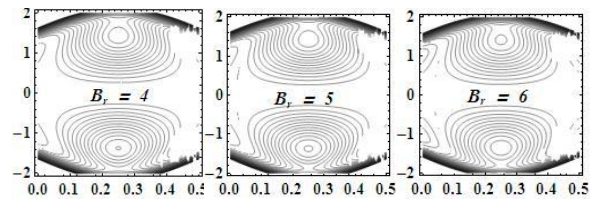


Fig.7.4: Stream line patterns for different values of B_r
($\epsilon = 0.5, \bar{Q} = 0.7, \bar{\alpha} = 5, N_t = 5, G_r = 6, \bar{\eta} = 1.1, N_b = 10, \alpha = 30^0$)

5 Conclusions

The major premise of the paper is Peristaltic transport of a couple-stress fluid with nanoparticles in an inclined tube with heat and mass transfer effects. The study particularly pertains to a situation when the Reynolds number is low and wavelength is large. Emphasis was laid to investigate the pressure drop characteristics, frictional force, temperature profile, nano particle phenomenon, heat transfer coefficient, mass transfer coefficient and streamline patterns of the couple-stress fluid parameters, Brownian motion parameter, thermophoresis parameter, local temperature Grashof number, local nano particle Grashof number and inclination. Homotopy perturbation method is used to solve the coupled equations of temperature profile and nano particle phenomena and analytical methods have been applied to the present study to find the other variables.

The main points of the analysis are as follows:

- i Pressure drop increases with the couple-stress fluid parameter $\bar{\alpha}$, Brownian motion parameter, local temperature Grashof number and with inclination. Pressure drop increases with the couple-stress fluid parameter $\bar{\eta}$ in the peristaltic pumping region ($0 < \bar{Q} < 0.38$) and decreases in the augmented pumping region ($0.42 < \bar{Q} < 1$).

The absolute value of the frictional force ($|\bar{F}|$) increases with couple-stress fluid parameter $\bar{\eta}$, thermophoresis parameter and with local Nano

- particle Grashof number but decreases with Brownian motion parameter, local temperature Grashof number and with inclination.
- iii Temperature profile increases with the increase of Brownian motion parameter and decreases with the increase of thermophoresis parameter. Value of temperature profile is maximum in the range $[-0.5, 0.5]$.
- iv Nanoparticle phenomena (σ) increases with the increase of Brownian motion parameter (N_b) and decreases with the increase of thermophoresis parameter (N_t) and it attains maximum value at $r = 0$.
- v Heat transfer coefficient increases with Brownian motion parameter and thermophoresis parameter, amplitude ratio (ϵ) and then decreases after attaining a constant value.
- vi Mass transfer coefficient increases with Brownian motion parameter, thermophoresis parameter and with amplitude ratio and then decreases after attaining a constant value.

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